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ermal Sciences Final Exam

Q3) In an ideal Rankine cycle, water leaves the boiler as saturated vapor at 90 C and it leaves the turbine with 90 % quality. If the condenser operates on 30 kPa .pressure and the mass flow rate of the fluid is 1 kg/sec

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 \mathbf{x}

Thermal Sciences Final Exam x +

1FAIpQLSfCUMKzgG5B77P8ErB8yYA1DwEQ1PNkYOxLF1zVjjZZ_q25NQ/formResponse

Q2) One kg of saturated water at 120 C, is completely condensed at constant ,pressure. If the surrounding temperature is 30 C

The entropy changes of the system (kJ/K) is 5.6 O -6.5 \bigcirc 6.5 \bigcirc -5.6 \bigcirc 改革 The net entropy change (kJ/K) is 1.9 \circ

The heat exchanged with surroundings (kJ) is

 -9.1

 -19 \circ

 9.1 \circ

Time left 0:44:16

 (1) σ

Quiz nav

13 14 14

Finish attent

Question 6 Not yet answered. to tuo Deltina 4.00

 $+100$ duestion The pump shown in the figure below has a head of 250 m. The difference in the elevation is 200 m. Pipe length and dimeter are 500 m and 0.075 m respectively. Note: pipe is smooth (i.e. roughness is zero). Assume water density 1000 kg/m³ and dynamic viscosity is 1.792x 10⁻³ kg/m·s

Purn

Presture

 -0.8

 $K_{\nu} = 1.5$

The Re number value is.

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 $\boldsymbol{\mathsf{x}}$

Thermal Sciences Final Exam

QLSfCUMKzgG5B77P8ErB8yYA1DwEQ1PNkYOxLF1zVjjZZ_q25NQ/formResponse

The inner and outer surfaces temperature of a furnace are 850 C and 250 C respectively. The wall is of thermal conductivity of 0.3 W/m.K and thickness of 50 cm. The thermal resistance (K/W) is

 x +

?In the shown composite wall, the junction is 150 C the ratio of wall thickness

$$
T_1 = 150 \text{ C}
$$

A A A

 $1:2$

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EXAMPLE 18-1 Temperature Measurement by Thermocouples

The temperature of a gas stream is to be measured by a thermocouple whose \blacksquare junction can be approximated as a 1-mm-diameter sphere, as shown in Fig. 18-9. The properties of the junction are $k = 35$ W/m-K, $\rho = 8500$ kg/m³, and $c_n = 320$ J/kg·K, and the convection heat transfer coefficient between the junction and the gas is $h = 210$ W/m²-K. Determine how long it will take for the thermocouple to read 99 percent of the initial temperature difference.

SOLUTION The temperature of a gas stream is to be measured by a thermocouple. The time it takes to register 99 percent of the initial ΔT is to be determined.

Assumptions 1 The junction is spherical in shape with a diameter of $D = 0.001$ m. 2 The thermal properties of the junction and the heat transfer coefficient are constant. 3 Radiation effects are negligible.

Properties The properties of the junction are given in the problem statement. Analysis The characteristic length of the junction is

$$
L_c = \frac{V}{A_c} = \frac{\frac{1}{6}\pi D^2}{\pi D^2} = \frac{1}{6}D = \frac{1}{6}(0.001 \text{ m}) = 1.67 \times 10^{-4} \text{ m}
$$

u

LK

Then the Biot number becomes

Final Exam $\boldsymbol{\mathsf{x}}$

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D.

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SfCUMKzgG5877P8ErB8yYA1DwEQ1PNkYOxLF1zVjjZZ_q25NQ/formResponse

The power produced by the turbine [kW] is

Power requited by the pump (kW) is

 1720 O

 172 O

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뫄

 $\mathbf x$

Thermal Sciences Final Exam

e/1FAlpQLSfCUMKzgG5B77P8ErB8yYA1DwEQ1PNkYOxLF1zVjjZZ_q25NQ/formResponse

A wall of thickness 0.6 m and $k = 17.45$ W/m K. if the first face is subjected to radiant heat at a rate of 530.5 watt/m2 while the second face is kept at of 38C, The temperature of the first face (C) is

 $x +$

 32° 32.87 O 87.5 \bigcirc 47.08 0

The ratio of the conducted heat through two walls of the same thickness and cross sectional with one wall of thermal conductivity equals to half of the other one is HOHAL H

> $1/2$ \bigcirc 4 2

4 3-m-wide, 8-mhigh rectangular gate is located at :he end of a ectangular passage that is connected to a open tank arge filled with water as shown in Figure. The gate is hinged at its bottom and

held closed by a

norizontal force, $F_{\mu\nu}$ located at the center of the gate. The water depth, h, above the center of the gate, when the water depth, h is 15 m. Note that the density of water: = 999 kg/

) The hydrostatic pressure force on the gate is:

- a. 3528 kN
- b. 1764 kN
- c. 147 kN
- d. 3214 kN
- e. None of the above
-) The center of pressure measured from the free surface of the water along the plane of the gate is:
	- a. 7.86 m
		-

 $b. 15.36 m$ c. 5.33 m $d. 16.75 m$ e. None of the above

) The minimum force F_{μ} when the gate start to open is: a. 3528 kN b. 1764 kN

c. 147 kN

d. 3214 kN

e. None of the above

$Q(2-4)$

A 200-kg. 5-m-wide rectangular gate shown in the figure is hinged at B and leans against the floor at A making an angle of 45° with the horizontal. The gate is to be opened from its lower edge by applying a normal force at its center. Assume the density of the water is 1000 kg/m3. Answer Problems (2-4):

Ξi

a

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The heat added to fluid within boiler [kW] is

 -4220 \bigcirc

 \mathbf{r}^{R}

The water level in a tank is 20 m above the ground. A hose is connected to the bottom of the tank, and the nozzle at the end of the hose is pointed straight up. The tank cover is airtight, and the air pressure above the water surface is 2 atm gage. The system is at sea level. Note that $(1 atm = 101.325 kPa)$ and the density of water = 1000 kg/m³. The maximum height to which the water stream could rise is:

 $f. 30.3 m$

g. 51.0 m

 $h.40.7 m$

 $i. 31.0 m$

j. None of the above

Thermal and Fluid Sciences (0904248) ... (Thermal-Fluid sciences Spring 2020)

$Q(8-9)$

Air

 $\mathbf{8}$

 \Box

 \circ

Air flows through a pipe at a rate of 0.3 m3/s. The pipe consists of two sections of diameters 20 cm and 10 cm with a smooth reducing section that connects them. The pressure difference between the two pipe sections is measured by a water manometer. Neglect the frictional effects and take the air density to be 1.20 kg/m3. Answer Problems (8-9):

 $\overline{2}$

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 20 cm

 \bigcirc

3

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Question 2

 $5 - 3$

Not yet answered

Marked out of 2.00

 P Flag question

> Water with density 1000 kg/m³ enters a hydraulic turbine through a 30-cm diameter pipe at a rate of 0.6 $m³/s$ and exits through a 25-cm diameter pipe. The pressure drop, ΔP , of water in the turbine is measured to be 200 kPa. Assume kinetic energy correction factor, α =1. For a combined turbine-generator efficiency of 80 percent. The velocity at the exit of the turbine is:

Select one:

- O a. None of the above
- O b. 38.3 m/s
- O c. 6.1 m /s
- O d. 8.49 m/s
- $e.12.2 m/s$

Clear my choice

Test name: Quiz#2

Question 1/1

For the given system below, the flow rate is 1.25 m3/sec and the valve is half open. Find:

1. Re number and the flow type.

 $1 - 5 - 1$

- 2. friction factor
- 3. the value of Z_2 in meters $T \in \bigcap_{n=1}^{\infty} V$

10 cm diameter steel pipe

Threaded clhows

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MEAIpQLSfCUMKzgG5B77P8ErB8yYA1DwEQ1PNkYOxLF1zVjjZZ_q25NQ/formResponse

Lumped capacitance methods state that thermal conductivity is

 $x +$

Infinitely small O Moderate \bigcirc 50% small (Infinitely large \bigcirc

The time required to cool a 2 mm diameter sphere is to be cooled from 500 to 60 C by exposing it to an environment at 25 C. Given the following (Density = 2250) kg/m3, Specific heat = 850 J/kg K, Conductivity = 1.5 W/m K), The time required to achieve this in seconds is

> 16.78 \bigcirc 15.78 13.78 \bigcirc 14.78 \bigcirc

 $1⁰$

 $\pi^{\!R}$

3.13 A house has a composite wall of wood, fiberglass insulation, and plaster board, as indicated in the sketch. On a cold winter day, the convection heat transfer coefficients are $h_a = 60$ W/m² K and $h_i = 30$ W/m² K. The total wall surface area is 350 m².

A manometer is attached to a pipe as shown. The specific weight of the flowing fluid,, the specific weight of the gage fluid,, and the various heights shown. For, , and . Note that. The value of the pressure drop, is:

Question 20 Not yet answered

Marked out of 2.00 P Flag question

Answer:

The rate of convection heat transfer from one steel ball (rounded to two decimal digits) at the end of the process in W is:

question

The thermal resistance of the inside air (rounded to four decimal digits) in \degree C/W is:

Answer:

Question 5 Not yet answered Marked out of 4.00 F Flag

question

The velocity in the outlet pipe from this reservoir is 10 m/s and $h = 25$ m. Assume negligible friction and viscous effects. Under these conditions. Assume the water density is 1000 kg/m³.

Question 6 Not yet answered Marked out of 2.00 P Flag question

Water is pumped from the lower reservoir to the upper reservoir at a rate of 0.25 m^3/s . The inlet is slightly rounded $(r/D = 0.1)$, the exit is sharp-edged, the bend is smooth and flanged, the pipe is made of cast iron, and the pump efficiency is 80%. Assume the water density, ρ , is 1000 kg/m³ and the dynamic viscosity, μ , of the water is 10^{-3} kg/m.s.

The major head losses (rounded to two decimal digits e.g. 1.24), in m is:

Answer:

Question 6 Not yet answered Marked out of 2.00 P Flag question

Water is pumped from the lower reservoir to the upper reservoir at a rate of 0.25 m^3/s . The inlet is slightly rounded $(r/D = 0.1)$, the exit is sharp-edged, the bend is smooth and flanged, the pipe is made of cast iron, and the pump efficiency is 80%. Assume the water density, ρ , is 1000 kg/m³ and the dynamic viscosity, μ , of the water is 10^{-3} kg/m.s.

The major head losses (rounded to two decimal digits e.g. 1.24), in m is:

Answer:

Question 3 Not yet answered Marked out of 3.00 F Flag question

The gate shown is circular with diameter 6 m. Let the weight of the gate be 100 kN. Assume the water density is 1000 kg/m³.

Not yet answered Marked out of 5.00 P Flag

Question 4

question

Question¹

Not yet answered

Marked out of 3.00

 P Flag question

For the closed tank with pressure gages readings of $P_A = 20$ kPa, and $P_B = 27.5$ kPa. Assume the water density is 1000 kg/ m^3 .

The specific gravity of the oil (rounded to three decimal digits e.g. 1.278), is:

 P_A

 P_B

 P_C

Answer:

Question 2 Not yet answered Marked out of 4.00 P Flag

question

The pressure reading on gage C (rounded to two decimal digits), in kPa is:

Answer:

Ouestion¹⁸ Not yet answered Marked out of 2.00

 P Flag question Steel balls 12 mm in diameter are annealed by heating to $1150 K$ and then slowly cooling to 400 K in an air environment for which $T_{\infty} = 325 \text{ K}$ and $h = 20 \text{ W/m}^2 \cdot \text{K}$. Assuming the properties of the steel to be $k = 40$ W/m·K, $\rho = 7800 \text{ kg/m}^3$, and $c = 600 \text{ J/kg} \cdot \text{K}$

The time required for the cooling process in s is:

Answer:

Answer:

Question 19 Not yet answered

Marked out of 2.00

 P Flag question The total amount of heat transfer from one steel ball (rounded to two decimal digits) in J is:

Question 1 Not yet answered Marked out of 3.00

 P Flag question For the closed tank with pressure gages readings of $P_A = 20$ kPa, and $P_B = 27.5$ kPa. Assume the water density is 1000 kg/ m^3 .

The specific gravity of the oil (rounded to three decimal digits e.g. 1.278), is:

Answer:

$(COP)_{R}^{-27}$ $(COP)_{11} = (CP)_{12} + 1 = 28$ (COP) R = QL O

$$
CoP = \frac{T_1}{T_2 - T_2 1} = \frac{297}{308 - 297}
$$

$$
T_1 = 297K
$$

$$
T_2 = 308
$$

 $Q.3$

Cop) = 87 = 4 KW Minput = 0-148 KW heat rejected (d) $QR = Q_L + \text{Winput}$ $QR = 4.148KU$ 0-148KW power input = (b)

Given, intet conditions. $P_1 = 690$ K Pa $T_1 = 300$ K

 $S₀₁$

W

B

B

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VS

V

 \mathcal{Q}

 \mathbb{Z}

S

 $\tilde{\omega}$

G

 \mathfrak{D}

 $\ddot{}$

 \vec{v}

 Ext ¹ condition. $P_2 = 127$ KPa $T_2 = 252$ K $V_2 = 320$ m/s

Assuming mass-flow rate (m) at inlet and exit remains constant,

 \bigodot

$$
m = \frac{AV_1}{V_1} = \frac{(AV_2)}{V_1}
$$
\n
\n
$$
P_1 \underbrace{(AV_1)}_{I \nmid K \nmid U_1} = \frac{P_2(AV_2)}{P_1(AV_2)}
$$
\n
\n
$$
V_1 = \underbrace{(P_2 V_2)(T_1)}_{T_2} (T_1)
$$

Substituting with valuel given, i.e. \rightarrow a a $V_1 = \left(\begin{array}{c} 127 & x & 320 \\ 2 & 52 \end{array}\right) \cdot \left(\begin{array}{c} 300 \\ 690 \end{array}\right)$ $\{V_{1} = To - 12 \text{ m/s.}\}$ $\frac{1}{2}$ σ inter velocity of Air is 70.12 m/s. Any -3

 $q_{end} = \frac{\kappa A}{1} (\frac{\tau_{ter}}{\sqrt{2}} \tau_{g})$ 96π , $0.035A (290-43)$ $q_{int.} = 8.645 A$ Heat transfer by convection =) $q = \hbar A (\overline{4} - \overline{7}_2)$ $q = 12 \times A \times (43 - 33)$ $\left(\begin{array}{c|c} 1 & q & =120A \\ \hline \end{array}\right)$ $\%$. Thend, $=$ $\%$ conv. $720.072m$ $8.645A = 120A$ $L = 7.2$ cm Tnsulation thickness = 7.2 Cm

From eq(1)

 L_{124} = Kins $\left(A R_{16} - \frac{L_{5f}}{K_{5f}} - \frac{1}{44}\right)$ $= 0.014 \times (1.8 \times 0.25 - \frac{3 \times 10^{-3}}{0.3} - \frac{1}{2+5.9})$

 $= 0.0044m$ $L_{\mathsf{r}} = 4.4 \text{mm}$

major head loss = O'O171 X500 x 278142 2 x 9.81 00075 244.95M Aus minor head loss= 12.8 x 2.78422

 $=5.0U+m_{AB}$

 $P_1 = P_2$ $V_1 = V_2$

$$
200 = 200 + \frac{41.0^{2}}{29d} + 12.8\frac{10^{2}}{29}
$$
\n
$$
50 = \left(\frac{4 \times 50}{2 \times 981 \times 00 + 5} + \frac{12.8}{2 \times 981}\right) 10^{2}
$$
\n
$$
\frac{12021 - 1}{x} \text{ assuming } 10x0 \text{ is } + \text{subular}
$$
\n
$$
8 = \frac{1000}{R_{\text{e}}}(x + 5 = 0.039 + 3 \text{ (1000 } R_{\text{e}} \cdot 10^{5})
$$
\n
$$
9 = 1.8496 \text{ m/s}
$$
\n
$$
R_{\text{e}} = \frac{9 \text{yd}}{44} = \frac{10^{3} \text{ x } 1.8496 \times 0.045}{1.492 \times 10^{-3}}
$$
\n
$$
R_{\text{e}} = \frac{9 \text{yd}}{44} = \frac{10^{3} \text{ x } 1.8496 \times 0.045}{1.492 \times 10^{-3}}
$$
\n
$$
R_{\text{e}} = \frac{48666.29 \text{ ft}}{4.492 \times 10^{-3}}
$$
\n
$$
R_{\text{e}} = 48666.29 \text{ ft}
$$
\n
$$
R_{\text{e}} = 48666.29 \text{ ft}
$$
\n
$$
9 = 2.668 \text{ ft}
$$

Re= 1115033.2081

 $f = 0.0173$ $9 = 2.7670$ mlz

 $Re = 115806.3616$

$$
f=0.0171
$$

\n
$$
\frac{102.2.7814 \text{ m/s}}{Re=116409.040} \text{ days}
$$

 $\frac{T-T_{i}^{*}}{T_{o}-T_{i}^{*}} = e^{-\left(\frac{hAs}{PVC_{P}}\right)xT}$ Roperties of warter at $\circ \times$ = 999.8 by m³
 C_{ρ} = 4217 J Hy.k
 $0 - 25$
 $C = \frac{4 \times 3}{2 \cdot 5 \times 10^{-2} \times 999.8 \times 4217} \times T$ $P = 2955.45$ see T_{τ} = 49.25 minutes

 \Rightarrow

n
R

nn ann ann

f-dacy's furction factor. myör head loss ochez = Lev minor loss (hu) $2 = 0.8 \frac{10^2}{29} + 5x \frac{10^2}{29} + 4x1.5x \frac{10^2}{29} + 1.0 \frac{10^2}{29}$ $M_{2} = 12.8 \frac{10^{2}}{29}$ $(bu) = f \frac{1}{2}gd$ $d = 0.075m$ 22-21-2007), L=50077 $Hp = 250m$ $9-1000$ kg/m³, 8724782 , 11313210^{3} kg/m-8 APPL4 Bernoulies bequation dw 060 $\frac{p_1}{r_0} + \frac{v_1^2}{r_0} + 2t + Hp = \frac{p_2}{r_0} + \frac{v_2^2}{r_0} + 2t + h_1 + (h_1)^2$

Now Finding Ts $T_S = T_f - (100) \times Lsg$
Kef A $= 35^{\circ}$ c - 100 x 3x10⁻³ = 34.4 °C 0.3×1.8 $T_S = 34.4^{\circ}C$

